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4 **Explosion behavior of methane - dimethyl ether /air mixtures**  
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# Explosion behavior of methane - dimethyl ether /air mixtures

Bo Zhang , Hoi Dick Ng

## Abstract

In this study, the effect of dimethyl ether (DME) addition on the explosion of methane/air mixture is investigated. In particular, the explosion and deflagration parameters of various CH<sub>4</sub>-DME/air mixtures are systematically studied. Those parameters include flammability limits, maximum explosion pressure,  $p_{\max}$ , maximum rate of pressure rise  $(dp/dt)_{\max}$ , and laminar burning velocity  $S_L$ . In general, the experimental results indicate that both  $p_{\max}$  and  $(dp/dt)_{\max}$  increase with increasing DME content in the total fuel. Simple correlations to evaluate the dimensionless pressure ( $\bar{p}$ ) of CH<sub>4</sub>-air and DME-air mixtures with an initial pressure of 100 kPa are developed and given respectively by  $\bar{p} = 1/[2.81839+0.22424\chi_{\text{CH}_4}-2.14347\ln(\chi_{\text{CH}_4})]$  and  $\bar{p} = 1/[1.04153+0.12637\chi_{\text{DME}}-0.94532\ln(\chi_{\text{DME}})]$  where  $\chi$  is the volume fraction of the fuel. The experimental results also indicate that for lean CH<sub>4</sub> mixtures, the relationship between  $p_{\max}$  and DME concentration exhibits an inversely “U-shaped” curve. In contrast, an exponential decay of  $p_{\max}$  with increasing DME concentration is observed for rich CH<sub>4</sub> mixtures. By adding DME into the CH<sub>4</sub>-air mixture, both the lower and upper flammability limits go down. The maximum amount of the total fuel for the binary blend (CH<sub>4</sub> plus DME) below which the mixture can be initiated is approximately 15~16%. Lastly, a good agreement is found in the determination of the laminar burning velocity  $S_L$  using both a theoretical model and the CHEMKIN-PREMIX simulation. For CH<sub>4</sub>-DME/air mixtures, the  $S_L$  near the stoichiometric equivalence ratio  $\phi_{\text{total}} = 1$  is larger than the fuel lean or rich side. It is found that with a slight amount of DME adding into the lean CH<sub>4</sub> mixture, making  $\phi_{\text{total}}$  closer to stoichiometry, the value of  $S_L$  increases. However, with further addition of DME into lean CH<sub>4</sub> mixture, or DME adding into rich CH<sub>4</sub> mixture, only a decreasing behavior of  $S_L$  is observed.

**Keywords:** Dimethyl ether addition; Maximum explosion pressure; Maximum rate of pressure rise; Flammability limits; Laminar burning velocity

## 67 **1 Introduction**

68 Alternative fuels with the properties of high-efficiency and low-emission combustion, have  
69 received particular interests because of the rapid increase in energy consumption and increasingly  
70 stringent emission regulations. Among them, natural gas (NG) is one of the most widely used  
71 alternative fuels for automobiles and has long been considered as a promising alternative fuel due to  
72 its favorable chemical characteristics, such as: high H/C ratio, large octane number, and especially  
73 its low emissions [1-3]. Methane  $\text{CH}_4$  as an environmental-friendly fuel and the main component of  
74 NG produces less carbon dioxide for each unit of heat released, but more heat per mass unit than  
75 other complex hydrocarbons. Nonetheless, methane has some drawbacks regarding its combustion  
76 properties, e.g., long ignition delay time, low flame speed, low ignitability and narrow flammability  
77 limit range. All of these pose great challenges for its wide utilization in combustion engines [4].  
78 However, using more reactive fuel additives, the ignition and combustion performance of methane  
79 could be greatly enhanced. From studies conducted by Dagaut [5, 6] and Yao et al. [7, 8] on the  
80 detailed chemical mechanism for low and high temperature DME oxidation and the effect of DME  
81 addition to methane for homogeneous charge compression ignition (HCCI) engines, respectively,  
82 DME has shown promise as an effective promoter of high temperature methane ignition. Due to an  
83 increasing interest in using NG in the automotive industry, a thorough understanding of the  
84 fundamental explosion and combustion characteristics of DME-added mixtures is therefore  
85 important for developing advanced, NG-based, combustion engines and corresponding operating  
86 strategies [4].

87 Fundamental combustion properties, such as laminar flame speed and Markstein length, have  
88 been extensively studied in the past for methane- [9-11] and DME-air mixtures [12-18]. Many  
89 studies have been performed on  $\text{CH}_4/\text{H}_2$  or  $\text{CH}_4/\text{DME}$  binary fuel blends regarding the ignition  
90 delay time [4, 19-22], internal combustion engine ICE performance [23-25], and laminar flame  
91 speed [26-28]. The effects of DME addition on the high temperature ignition and burning properties  
92 of methane-air mixtures were also studied experimentally and numerically [19]. Premixed and

93 non-premixed ignition of methane/DME binary fuel blends with hot air has been studied through  
94 numerical simulation with detailed chemistry and various thermodynamic as well as transport  
95 properties [4].

96 While the combustion characteristics of methane mixtures with DME addition have been  
97 studied extensively, comparatively little explosion safety data, e.g., maximum explosion pressure,  
98  $p_{\max}$ , maximum rate of pressure rise  $(dp/dt)_{\max}$ , flammability limits, and laminar burning velocity  $S_L$ ,  
99 are currently available. In fact, the explosion hazard of CH<sub>4</sub>-DME mixtures, within storage  
100 infrastructures, is high due to the large destructive energy release associated with the combustion  
101 phenomenon. Therefore, in this study, experiments are performed systematically to address the  
102 explosion safety problems of CH<sub>4</sub>-DME/air mixtures by recording overpressure histories at  
103 different composition of CH<sub>4</sub> and DME in a standard 20-L spherical vessel and analyzing various  
104 derived explosion parameters. The data obtained in this study can contribute to a better  
105 understanding of the explosion behavior of CH<sub>4</sub>-DME/air mixtures.

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## 108 **2 Experimental details**

109 Measurement of the explosion parameters in CH<sub>4</sub>-DME/air mixtures were carried out in a standard  
110 20-L explosion spherical vessel according to the international standard ISO6184-1. A schematic of  
111 the apparatus is shown in Fig. 1. This facility was used previously for the same type of  
112 measurement for other gaseous fuels (e.g., natural gas) and detailed information of the experimental  
113 details can be found in [29]. In brief, the 20-L explosion spherical vessel consists of an explosion  
114 chamber, an electric ignition system, a control unit, a data acquisition system, a release valve, a  
115 vacuum pump and an air pump. A high-voltage electric spark was used to supply the ignition energy  
116 as in our previous studies [30-39]. The igniter was mounted at the center of the spherical bomb and  
117 a spark energy of 10 J, estimated from  $1/2 CV^2$  (“*C*” and “*V*” refer the capacitance and voltage,  
118 respectively.  $C = 0.1102 \times 10^{-3}$  F,  $V = 426$  Volts), was delivered by an electric ignition system.

119 For the explosion experiments, gas concentrations were regulated by the method of partial

120 pressure. The purities of the CH<sub>4</sub> and DME used in this experiment were 99.9% and 99.8%,  
121 respectively. The air used in the experiment is of 21% oxygen and 79% nitrogen (by volume). The  
122 experiments were performed at initial pressure of 100 kPa and temperature of 298 K. During the  
123 experiments, the explosion pressure evolutions were measured by a PCB pressure transducer  
124 installed in the vessel wall and recorded by a data acquisition system for each shot. These data  
125 yielded raw values of the explosion pressure and rate of pressure rise. In the present study, at least  
126 three shots were repeated at the same initial condition of the experiment, and five or more shots  
127 were made for the mixtures near LFL and UFL. Thus, the LFL and UFL were determined if half  
128 shots indicated explosion occur.

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### 131 **3 Results and discussion**

#### 132 **3.1 Maximum explosion pressure and maximum rate of pressure rise**

133 Samples of pressure traces obtained from experiments are shown in Fig. 2. In Fig. 2,  $p_{\max}$  occurs at  
134 the peak of the curve, however,  $(dp/dt)_{\max}$  represents the most steep of the curve, the maximum of  
135 those parameters do not occur at the same place. To characterize the mixtures,  $\lambda$  is defined as the  
136 ratio of DME over the total fuel (i.e., CH<sub>4</sub> plus DME) as follows:

$$137 \quad \lambda = \frac{C_{\text{DME}}}{C_{\text{DME}} + C_{\text{CH}_4}} \quad (1)$$

138 in which  $C_{\text{CH}_4}$  and  $C_{\text{DME}}$  denote the CH<sub>4</sub> and DME concentration, respectively.  $\lambda$  varies from 0 (pure  
139 CH<sub>4</sub>) to 1 (pure DME). Unless specified, the total fuel is at the stoichiometric concentration with air.  
140 It can be seen from Fig. 2 that the maximum explosion pressure  $p_{\max}$  increases with  $\lambda$ . It should be  
141 noted again that the  $\varphi_{\text{total}}$  (equivalence ratio of the overall fuels over air) is kept to 1 as  $\lambda$  changes.  
142 The slope of the pressure history is also observed to become more steep or in other words, the  
143 maximum rate of pressure rise  $(dp/dt)_{\max}$  increases as well with increasing  $\lambda$ . Figure 3 summarizes  
144 the  $p_{\max}$  and  $(dp/dt)_{\max}$  versus  $\lambda$  at an initial pressure  $p_0 = 100$  kPa. It shows clearly that  $p_{\max}$  and  
145  $(dp/dt)_{\max}$  increase with increasing DME content in the total fuel.

146 For pure CH<sub>4</sub>-air and DME-air mixtures, the maximum explosion pressure at different fuel  
 147 concentrations are shown in Fig. 4 and Fig. 5, respectively. The dimensionless pressure  $p_{\max}/p_0$  has  
 148 a maximum value slightly above the stoichiometric concentration ( $C_{\text{CH}_4} = 9.5\%$  at  $\varphi \sim 1.0$ ). The  
 149 experimental data and the curve fit of the dimensionless pressure at different CH<sub>4</sub> concentration are  
 150 shown in Fig. 4. The dimensionless pressure ( $\bar{p}$ ) at different CH<sub>4</sub> volume fraction is correlated by  
 151 the following equation:

$$152 \quad \bar{p} = \frac{1}{2.81839 + 0.22424x_{\text{CH}_4} - 2.14347\ln(x_{\text{CH}_4})} \quad (2)$$

153 where,  $\bar{p} = p_{\max} / p_0$ ,  $x_{\text{CH}_4}$  is the volume fraction of CH<sub>4</sub> in air. The coefficient of determination  $R^2$   
 154 equals to 0.9026. It should be noted that Eq. (2) is only valid for the initial pressure of 100 kPa and  
 155 temperature of 298 K. It is noteworthy that, although both  $C$  and  $\chi$  are essentially representing the  
 156 volume fraction,  $C$  denotes the volume fraction of one fuel (either DME or CH<sub>4</sub>) in  
 157 binary fuel blends, whereas,  $\chi$  is the fuel volume fraction for the mixture that contains only one  
 158 fuel.

159 A similar plot of the dimensionless pressure versus DME concentration at 100 kPa and 298 K  
 160 is shown in Fig. 5. The peak of  $p_{\max}$  appears at the DME concentration  $C_{\text{DME}}$  of 7%, which is  
 161 slightly larger than the stoichiometric concentration ( $C_{\text{DME}} = 6.54\%$  at  $\varphi = 1$ ). This behavior is  
 162 similar to the CH<sub>4</sub>-air mixture. The dimensionless pressure at different DME volume fraction is  
 163 given by the following expression:

$$164 \quad \bar{p} = \frac{1}{1.04153 + 0.12637x_{\text{DME}} - 0.94532\ln(x_{\text{DME}})} \quad (3)$$

165 where,  $x_{\text{DME}}$  is the volume fraction of DME in air, the coefficient of determination  $R^2$  equals to  
 166 0.9217.

167 Measurements of the maximum explosion pressure of CH<sub>4</sub>-DME binary fuel blends with air  
 168 are also performed in this study. In the experiment, the variation of the fuel composition was done  
 169 by adding or reducing the composition of DME, at a constant amount of CH<sub>4</sub> (e.g., 0%, 2%, 4%,

170 etc.) for each text matrix. The measured maximum explosion pressures for CH<sub>4</sub>-DME/air mixtures  
171 are shown in Fig. 6. Fig. 6a shows that the relation between  $p_{\max}$  and DME concentration is an  
172 inversely “U-shaped” behavior. The peak of each curve moves to the left side as the amount of CH<sub>4</sub>  
173 increases from 2 % to 8 %. Numerical values of these peaks are given in Table 1 and compared with  
174 the data of pure CH<sub>4</sub>-air and DME-air mixtures. It is found that the peak of  $p_{\max}$  occurs at an  
175 equivalence ratio of the total fuel  $\varphi_{\text{total}}$  slightly larger than 1 (i.e., between 1.08 to 1.22). For a  
176 mixture with a larger amount of CH<sub>4</sub> and less DME addition, the value of  $p_{\max}$  decreases.

177 However, as the equivalence ratio  $\varphi_{\text{CH}_4}$  is larger than 1, the relation between  $p_{\max}$  and DME  
178 concentration is completely different. An exponential decay curve is observed as shown in Fig.6b.  
179 This can be explained by the fact that adding DME makes the mixture even more fuel rich  
180 condition. For example, the values of  $\varphi_{\text{total}}$  are 1.77 and 1.66 for  $C_{\text{CH}_4} = 10\%$  with  $C_{\text{DME}} = 4\%$ , and  
181  $C_{\text{CH}_4} = 12\%$  with  $C_{\text{DME}} = 2\%$ , respectively. Consequently, the corresponding  $p_{\max}$  values become  
182 relatively small, merely of 0.32 MPa and 0.30 MPa, respectively.

183 The chemical equilibrium values of  $p_{\max}$  are obtained using the GASEQ equilibrium software  
184 [40] to compare with experimental results as shown in Figs.3-6. Large discrepancy can be seen as  
185 the condition of the LFL and UFL is approached. The theoretical maximum explosion pressure  
186 from GASEQ is based on the hypothesis of ideal adiabatic explosion without losses. As the  
187 composition approaches to fuel lean and rich sides, heat loss and also incomplete reaction can  
188 significantly affect the explosion process making the phenomenon non-ideal. It is thus expected that  
189 a large discrepancy occurs between the measured results from experiment with the calculation of  
190 ideal adiabatic explosion using chemical equilibrium [41]. For some cases, the experimental data of  
191  $p_{\max}$  are larger than that from GASEQ, e.g., near the stoichiometric condition of DME-air (see  
192 Fig.5). This may be possibly due to the error of experimental measurement and other possible  
193 transient effect. Nevertheless, these two sets of data are close if the measurement uncertainty is  
194 taken into account. In general, the GASEQ data are larger than experimental results at  
195 off-stoichiometric conditions.

196 The above analysis indicates that the behavior between  $p_{\max}$  and DME concentration depends  
197 on the equivalence ratio of CH<sub>4</sub>. For  $\varphi_{\text{CH}_4} < 1$ , the behavior exhibits an inversely “U-shaped” curve,  
198 whereas for  $\varphi_{\text{CH}_4} > 1$ , an exponential decay curve is found.

199

### 200 **3.2 Flammability limits**

201 At the ambient condition of 100 kPa and 298 K, the LFL and UFL of CH<sub>4</sub>/air determined from this  
202 study are 5% and 15%, respectively. For DME/air mixture, the LFL and UFL are 3.5% and 19%,  
203 respectively. It is noteworthy that the flammability limits for the CH<sub>4</sub>-air mixture obtained in this  
204 study agree well with the result published in a previous study (4.9% and 15.9%) [42]. For the  
205 DME-air mixture, Mogi et al.[43] reported that the flammability limits were 4% and 13% obtained  
206 using an explosion vessel with an internal volume of 180 L. A noticeable discrepancy is thus found  
207 on the rich limit, and the size of the chamber appears to be an influencing factor on the  
208 flammability limits, as argued by Zhang et al.[44]. This difference may be explained by the fact that  
209 in the small-scale apparatus, acoustic disturbance reflected from the chamber wall may generate  
210 turbulent fluctuations facilitating the flame propagation, hence prolonging the explosion limit.  
211 Other effect such as the mixture inhomogeneity and cooling effect for a higher volume in the large  
212 chamber vessel may also cause the observed discrepancy. It is worth noting that another study by  
213 Chen et al. [45] reported the flammability limits of 4% and 17% for DME-air mixtures using a  
214 smaller chamber, which indeed approach to the findings of this study.

215 Comparatively the flammability limits of DME/air are broader than CH<sub>4</sub>/air mixture. For  
216 blended CH<sub>4</sub>-DME/air mixtures, the results are tabulated in Table 2. It is found that the LFL and  
217 UFL of one fuel decreases with increasing amount of another fuel addition, e.g., as the addition of  
218 CH<sub>4</sub> increases to 4% in DME-air mixture, the LFL and UFL of DME decrease to 1% and 12%,  
219 respectively. For DME-air mixtures, the UFL is 19%. The presence of CH<sub>4</sub> in a binary fuel blend  
220 restricts the maximum amount of the total fuel below which the mixture can be initiated to  
221 approximately 15~16%, e.g., with 4%, 6%, 8% CH<sub>4</sub> addition, the maximum amount of DME so the



222 mixture can be initiated is 12%, 10% and 8%, respectively. Hence, these results show that CH<sub>4</sub> has  
223 a significant effect on the flammability of DME and controls the flammable range of the binary fuel  
224 blends.

225 Again, the experimental results indicate that the flammability limits for CH<sub>4</sub>-air mixtures at the  
226 initial condition of 100 kPa and 298 K are 5% for LFL and 15% for UFL. From the present data, it  
227 is interesting to note that the width of the flammable area (i.e., the difference between LFL and  
228 UFL) of the binary fuel blends is predominantly controlled by that of CH<sub>4</sub>-air. For example, only a  
229 shift rather than a widening or narrowing of the flammable range occurs as a small amount of DME  
230 is added into the CH<sub>4</sub>-air mixture. Equivalently, a small addition of CH<sub>4</sub> has a more prominent  
231 effect on the flammable range of the DME-air mixture. Without any CH<sub>4</sub> addition, it is already  
232 noted that the flammability limits of the pure DME-air mixture are 3.5% and 19%, comparatively  
233 wider than that of CH<sub>4</sub>-air. However, with just a small addition of CH<sub>4</sub> into the DME-air mixture, it  
234 is observed that the width of the flammable area reduces noticeably to that of CH<sub>4</sub> and further CH<sub>4</sub>  
235 addition results only in a displacement of the flammable range as in the case of DME addition into  
236 the CH<sub>4</sub>-air mixture.

237

### 238 **3.3 Laminar burning velocity**

239 The laminar burning velocity,  $S_L$ , represents the rate at which the flame front propagates into the  
240 unburned gas. It received particular attention not only because it is a basic physico-chemical  
241 property (e.g., reactivity, diffusivity, and exothermicity) of the premixed combustible gases [46], its  
242 accurate knowledge is also essential for engine design, modeling of turbulent combustion, and  
243 validation of chemical kinetic mechanisms. In addition, the determination of laminar burning  
244 velocity is very important for the analysis and calculations used in explosion protection [29].

245 Laminar burning velocity are computed using the PREMIX module of the CHEMKIN package  
246 [19, 41, 47-49], and alternatively by a theoretical model developed by Dahoe et al. [50, 51]. For the  
247 CHEMKIN-PREMIX simulation, the chemical kinetic mechanism involves 46 species and 263  
248 reaction [52]. In the previous work by Chen et al.[19], equivalent PREMIX calculations of the

249 laminar burning velocity for DME/CH<sub>4</sub>/air mixtures are performed, and results are in satisfactory  
 250 agreement with experimental data. As for the theoretical model, the laminar burning velocity  
 251 depends on  $p_{\max}$  and  $dp/dt$ . The model was also used in our previous study of natural gas-air  
 252 mixtures [29] and the mathematical expression is given by:

$$253 \quad S_L = \frac{1}{(p_{\max} - p_0)} \frac{1}{3} \left( \frac{4\pi}{3V} \right)^{-1/3} \left( \frac{p_0}{p} \right)^{1/\gamma} \left[ 1 - \left( \frac{p_0}{p} \right)^{1/\gamma} \times \left( \frac{p_{\max} - p}{p_{\max} - p_0} \right) \right]^{-2/3} \frac{dp}{dt} \quad (4)$$

254 where  $V$  is the vessel volume,  $p$  and  $p_0$  are the actual pressure and initial pressure, and  $\gamma$  denotes the  
 255 adiabatic coefficient of the unburned gas. Using Eq. (4) the value of the laminar burning velocity  $S_L$   
 256 is first calculated by the measured pressure time history (i.e., actual pressure  $p$  and  $dp/dt$ ) [51,  
 257 53-55] . The fitting of the data then yields the  $S_L$  at the reference initial condition  $P_0$ . Only the  $S_L$   
 258 data calculated at a flame radius greater than 6 mm are considered in order to avoid the distortion  
 259 and effects associated with spark ignition [26], so that it can be considered as an ideal spherical  
 260 flame propagating outward.

261 The laminar burning velocities computed by the above two methods for CH<sub>4</sub>-air and DME-air  
 262 at 100 kPa are given in Fig. 7. The computed results are also compared with other experimental  
 263 measurement. The experimental results for DME-air mixtures are taken from Daly et al. [13] and  
 264 Qin et al.[16]. For CH<sub>4</sub>-air mixtures, results from Chen et al. [19] are used for the comparison. It  
 265 can be seen from this plot both results agree well with each other. The values of  $S_L$  obtained from  
 266 the theoretical model given by Eq. (4) do not differ significantly from those computed by the  
 267 CHEMKIN-PREMIX simulation and previous experimental results.

268 Figure 8 shows the laminar burning velocities of CH<sub>4</sub>-DME/air mixtures at 100 kPa. For the  
 269 mixtures of  $\phi < 1$  (with fixed amount of  $C_{\text{CH}_4}$ = 2%, 4%, 6%, 8% for each data set), the laminar  
 270 burning velocity increases to a peak and subsequently decreases as the DME concentration  
 271 continues to increase. For the mixtures of  $\phi > 1$  (i.e.,  $C_{\text{CH}_4}$ = 10% and 12%), the laminar burning  
 272 velocity decreases rapidly as more DME is added. This is because for both CH<sub>4</sub>-air and DME-air,

273 the values of  $S_L$  are usually highest near stoichiometric conditions. Equivalently for CH<sub>4</sub>-DME/air  
274 mixtures, the value of  $S_L$  near  $\varphi_{\text{total}} = 1$  is generally larger than on the fuel lean or rich side as well.  
275 As a small amount of DME is initially added into the CH<sub>4</sub> lean mixture, the equivalence ratio of the  
276 total fuel-air mixture tends toward stoichiometry, which makes  $S_L$  increase. However, if more DME  
277 is added into the lean CH<sub>4</sub> mixture (or DME added into the rich CH<sub>4</sub> mixture),  $S_L$  decreases.

278

#### 279 **4 Concluding remarks**

280 A detailed investigation on the explosion behavior of methane - dimethyl ether /air mixture is  
281 performed in this study. The explosion and deflagration parameters including the maximum  
282 explosion pressure, maximum rate of pressure rise, flammability limits, and laminar burning  
283 velocity of the mixture are systematically measured and analyzed. Some conclusions are made as  
284 follows:

285 1.  $p_{\text{max}}$  and  $(dp/dt)_{\text{max}}$  increase with increasing DME content  $\lambda$  in the total fuel. For both  
286 CH<sub>4</sub>-air and DME-air mixtures, the dimensionless pressure at the equilibrium state has a maximum  
287 value at slightly above the stoichiometric concentration, and dimensionless pressure  $\bar{p}$  can be  
288 approximated by the correlations:  $\bar{p} = 1/[2.81839+0.22424\chi_{\text{CH}_4}-2.14347\ln(\chi_{\text{CH}_4})]$  and  
289  $\bar{p} = 1/[1.04153+0.12637\chi_{\text{DME}}-0.94532\ln(\chi_{\text{DME}})]$  at 100kPa, respectively.

290 2. The relation between  $p_{\text{max}}$  and DME concentration exhibits an inversely “U-shaped” curve  
291 for CH<sub>4</sub> lean mixture, and an exponential decay curve for CH<sub>4</sub> rich mixture. By adding the content  
292 of DME into CH<sub>4</sub>-air mixture, the flammability limits are slightly extended. The maximum amount  
293 of the total fuel (CH<sub>4</sub> plus DME) below which the mixture can be initiated is approximately  
294 15~16%.

295 3. The comparison of laminar burning velocity results between the CHEMKIN-PREMIX  
296 simulations and a theoretical model shows a satisfactory agreement for both CH<sub>4</sub>-air and DME-air  
297 mixtures at 100 kPa. For CH<sub>4</sub>-DME/air mixtures,  $S_L$  near  $\varphi_{\text{total}} = 1$  is larger than fuel lean or rich  
298 mixtures. As initially a small amount of DME is added into the lean CH<sub>4</sub> mixture, the mixture  $\varphi_{\text{total}}$

299 moves closer to 1 causing  $S_L$  to increase. Further additions of DME into the lean  $CH_4$  mixture, or  
300 any DME added into the rich  $CH_4$  mixture, only result in a decrease of  $S_L$ .

301

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420 **Tables**

421

422 Table 1 The compositions of CH<sub>4</sub> and DME and corresponding  $\phi$  at the peak value of  $p_{\max}$ 423 Table 2 Flammability limits of CH<sub>4</sub>-DME/air mixtures

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Table 1

CH <sub>4</sub> / % vol.	DME / % vol.	$\phi_{\text{total}}$	$p_{\max}$ / MPa
0	7	1.08	1.08
2	6.5	1.22	0.94
4	5	1.20	0.88
6	3	1.10	0.85
8	2	1.16	0.78
10	0	1.06	0.80

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Table 2

CH <sub>4</sub> %vol.	LFL(DME) %vol.	UFL(DME) %vol.	DME %vol.	LFL(CH <sub>4</sub> ) %vol.	UFL(CH <sub>4</sub> ) %vol.
0	3.5	19	0	5	15
2	3	14	1	4	14
4	1	12	3	2	12
6	–	10	5	0	10
8	–	8	6.5	–	8
9.5	–	6	7	–	8
10	–	6	9	–	6
12	–	3	11	–	4
14	–	1	13	–	2
15	–	–	15	–	1

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435 **Figure captions**

436  
437 Fig.1 The 20-L explosion spherical vessel (1 = DME, 2 = CH<sub>4</sub>, 3 = air)

438 Fig.2 Typical pressure trajectories for different CH<sub>4</sub> and DME compositions

439 Fig.3  $p_{\max}$  and  $(dp/dt)_{\max}$  as a function of ratio  $\lambda$

440 Fig.4  $p_{\max}$  as a function of CH<sub>4</sub> concentration at 100 kPa

441 Fig.5  $p_{\max}$  as a function of DME concentration at 100 kPa

442 Fig.6  $p_{\max}$  as a function of DME concentration with different CH<sub>4</sub> composition, (a)  $\varphi_{\text{CH}_4} < 1$ , (b)

443  $\varphi_{\text{CH}_4} > 1$

444 Fig.7 Comparison of the laminar burning velocity from different methods for CH<sub>4</sub>-air and DME-air

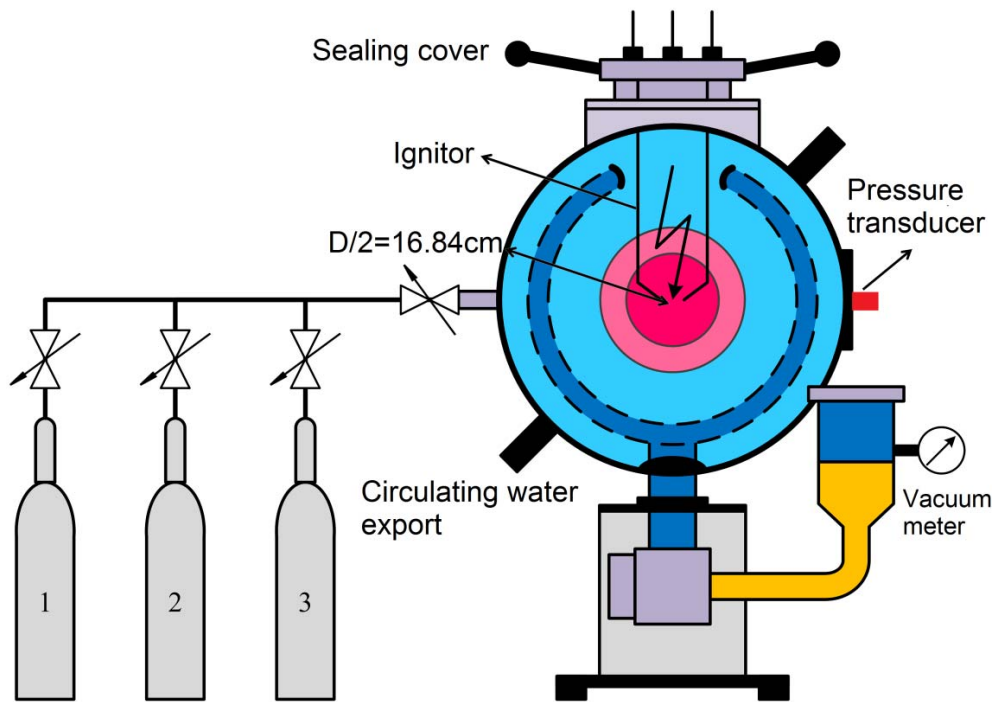
445 mixtures

446 Fig.8 Laminar burning velocity of CH<sub>4</sub>-DME/air mixtures

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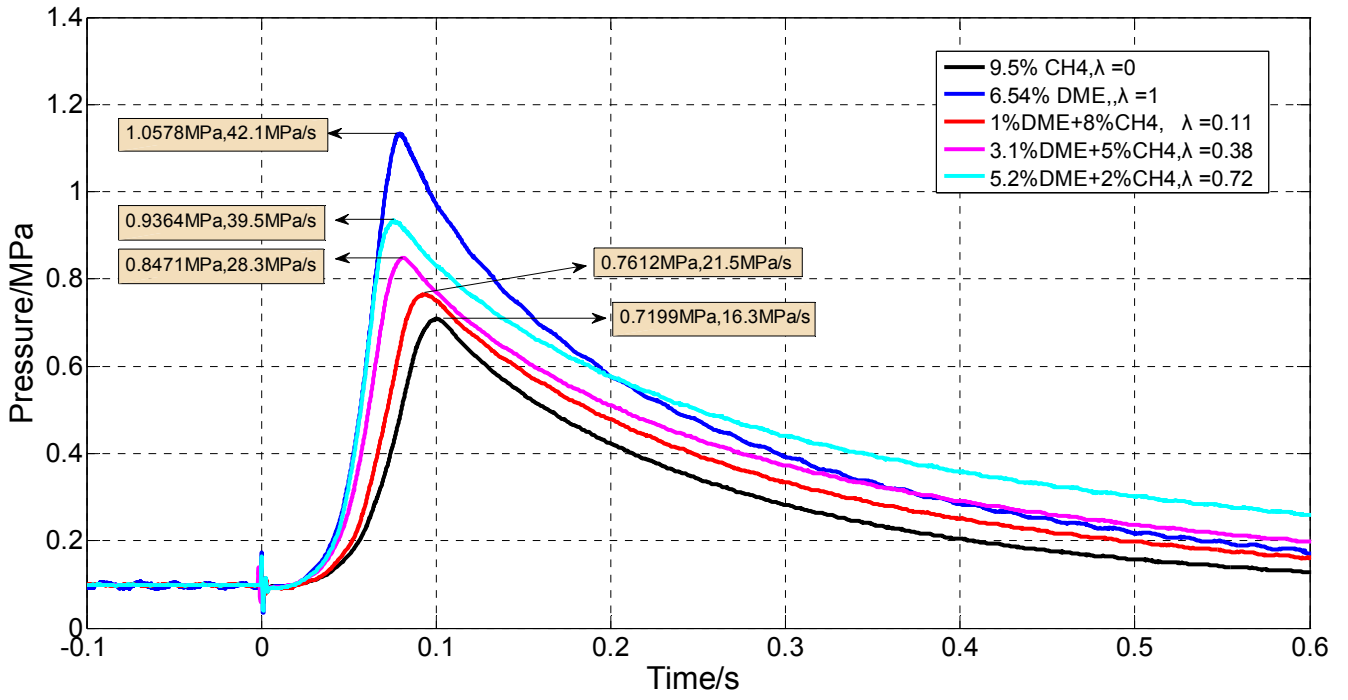
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Fig.1

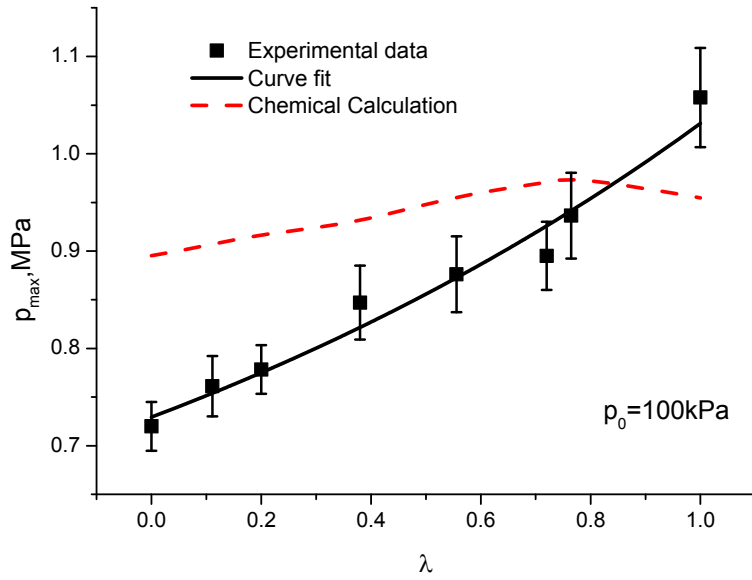
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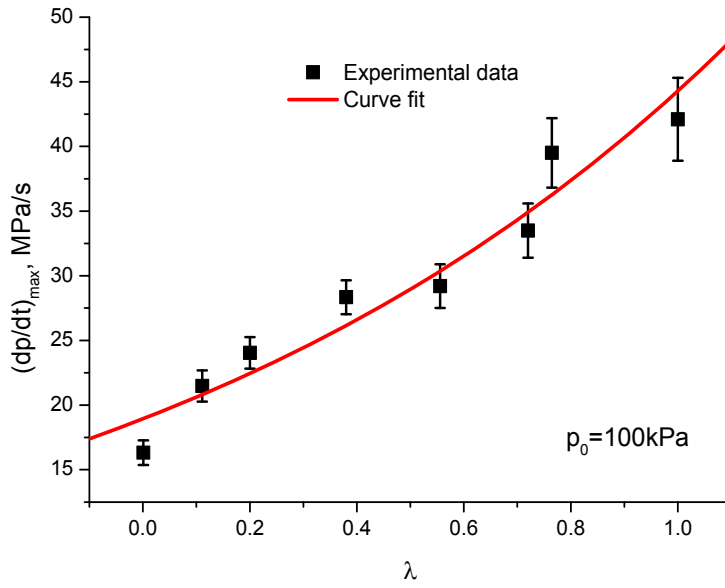
Fig.2

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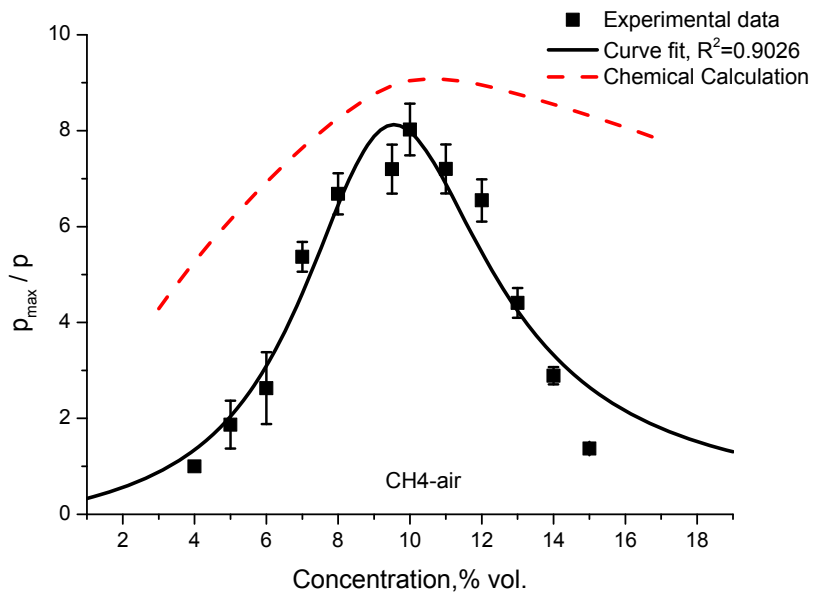
(a)



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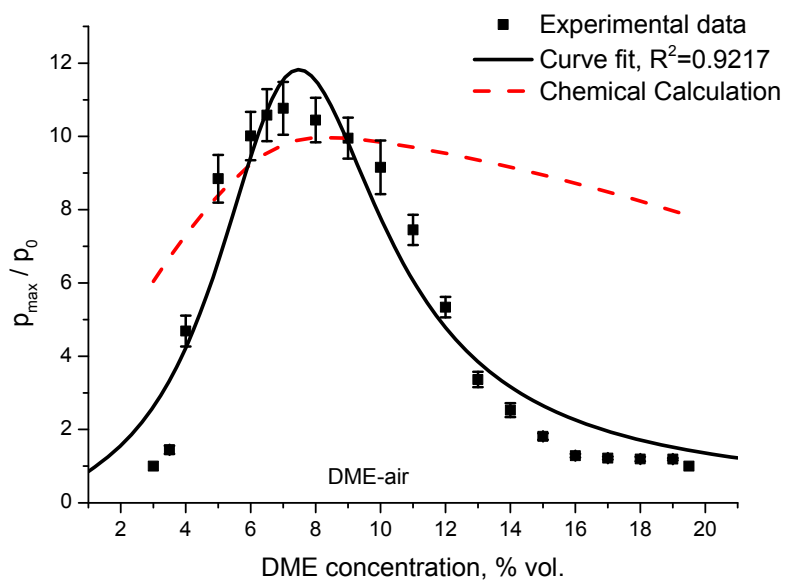
(b)  
Fig.3

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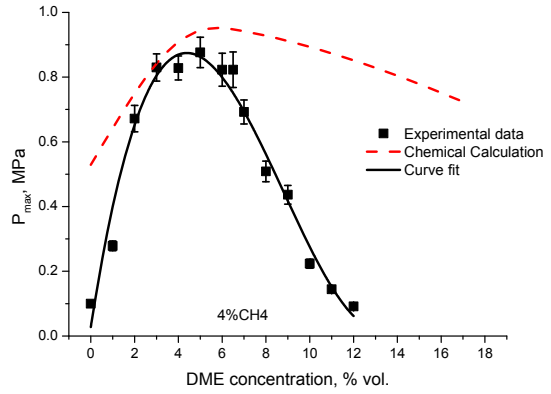
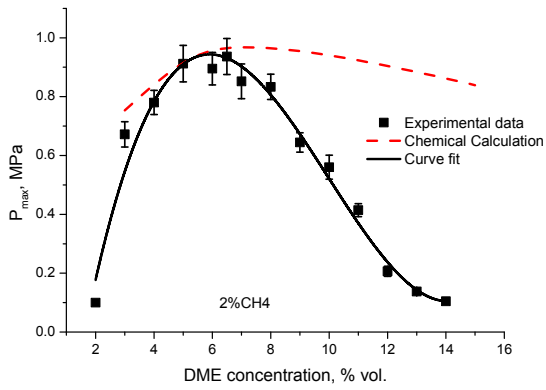
Fig.4



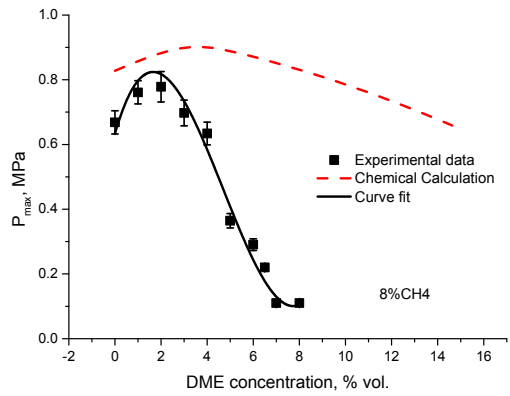
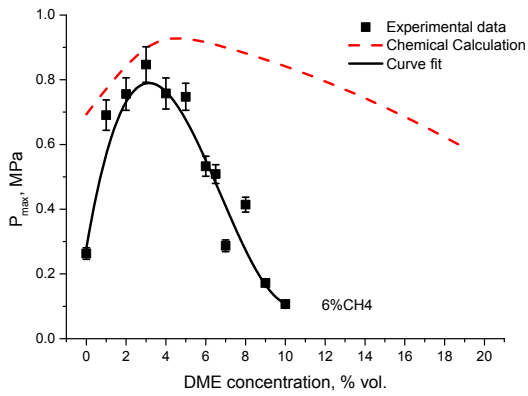
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Fig.5

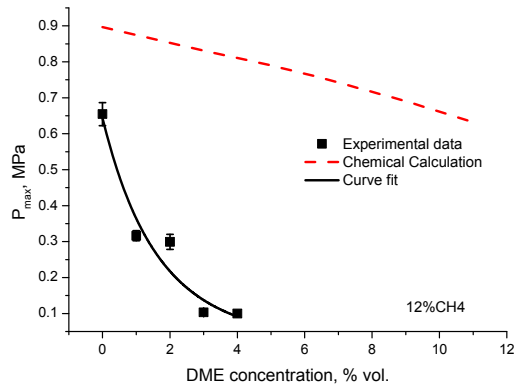
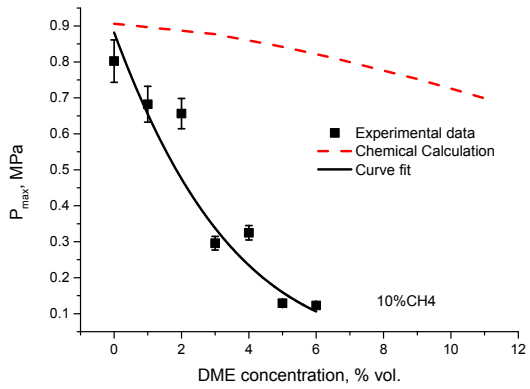
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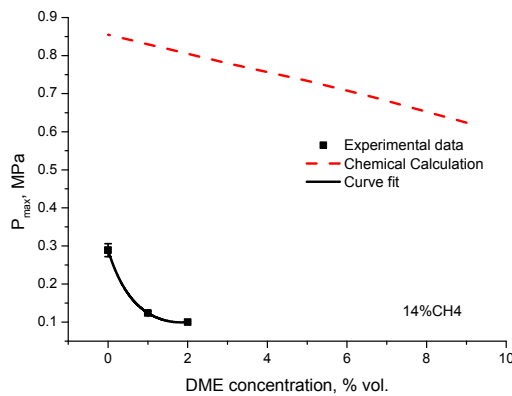
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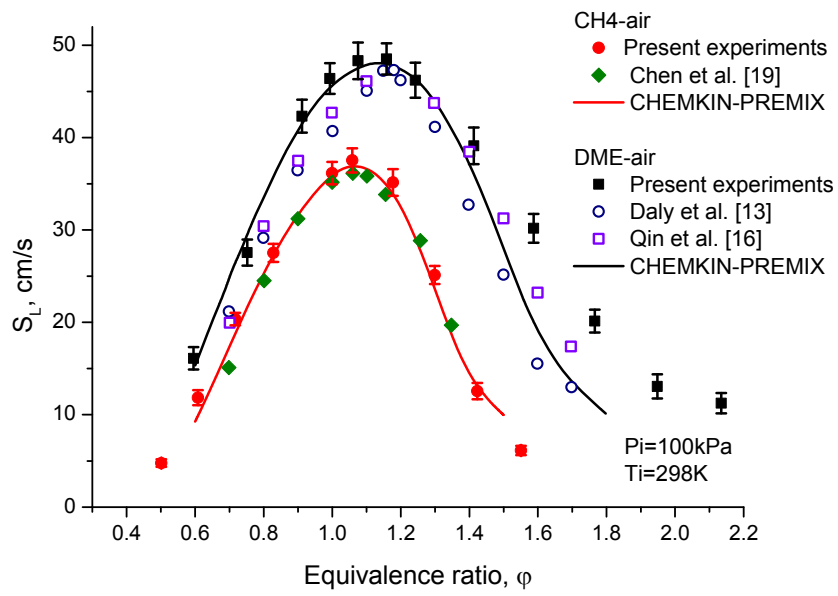


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Fig.6



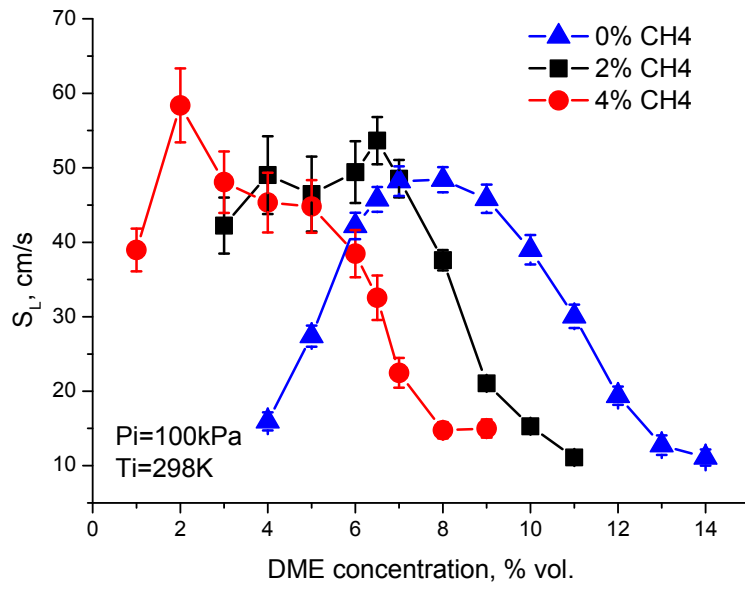
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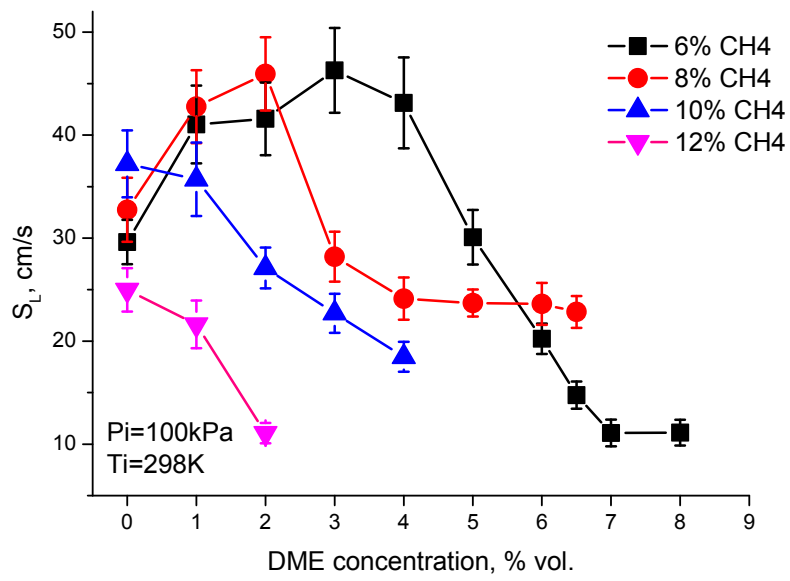
Fig.7

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(a)



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(b)

Fig.8